Fig. 1 : Effect of the support for the catalytic elimination of N_2O
VVH = 35000 h^{-1}; 3% 0_2, 2000 ppp N_20, 2000 ppm NH_3, temperature increasing (5°C/min)

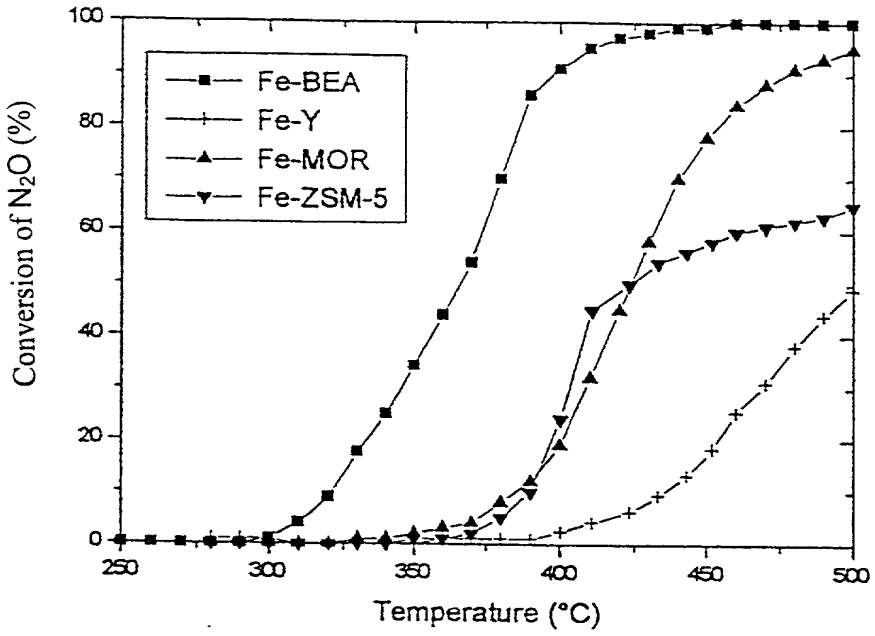

Fig. 2a : Influence of the presence of NH_3 on the catalytic elimination of N_2O in the presence of 3% O_2, VVH =35000 h^{-1}, 3% O_2, 2000 ppm N_2O, He.

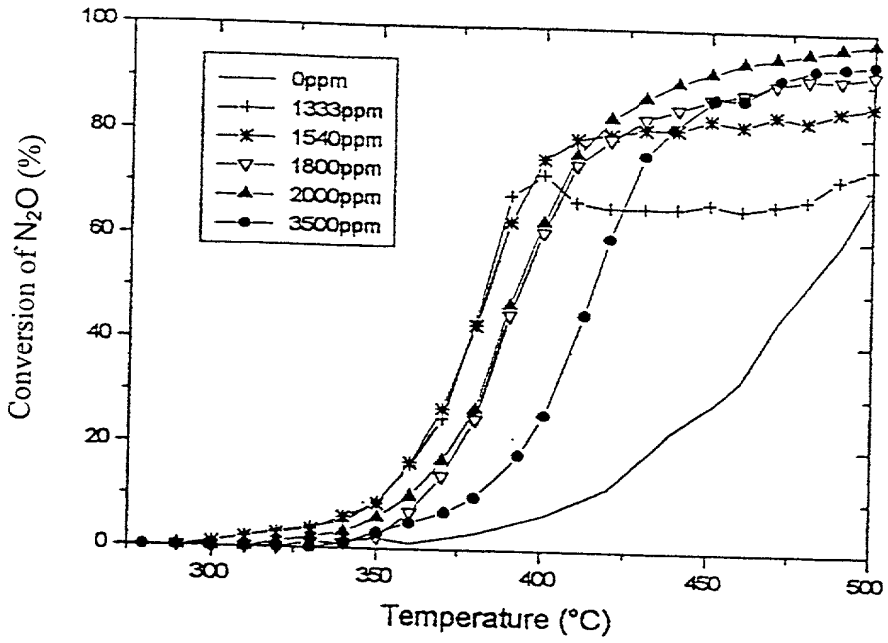

Fig. 2b1: Influence of the NH_3 content on the SCR of N_2O + NO Effect on the NO conversion of N_2O; VVH =35000 h^{-1}; 3% O_2, 2000 ppm N_2O, 500 ppm NO, x ppm

Catalyst: Fe(49) BEA_e; temperature increasing (5°C/min)

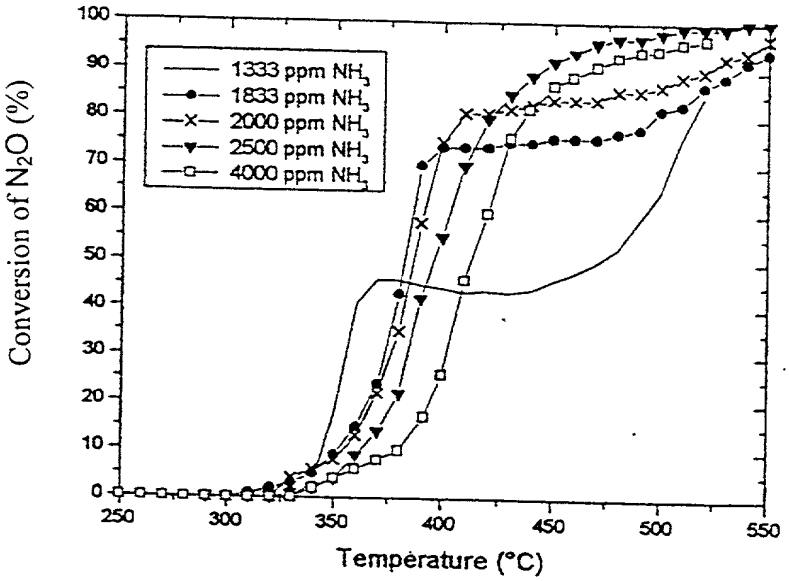

Fig. 2b2: Influence of the NH_3 content on the SCR of N_2O + NO: Effect on NO conversion

VVH =35000 h^{-1}; 3% O_2, 2000 ppm N_2O, 500 ppm NO, x ppm NH_3, He

Catalyst: Fe (49) BEA_e; temperature increasing (5°C/min)

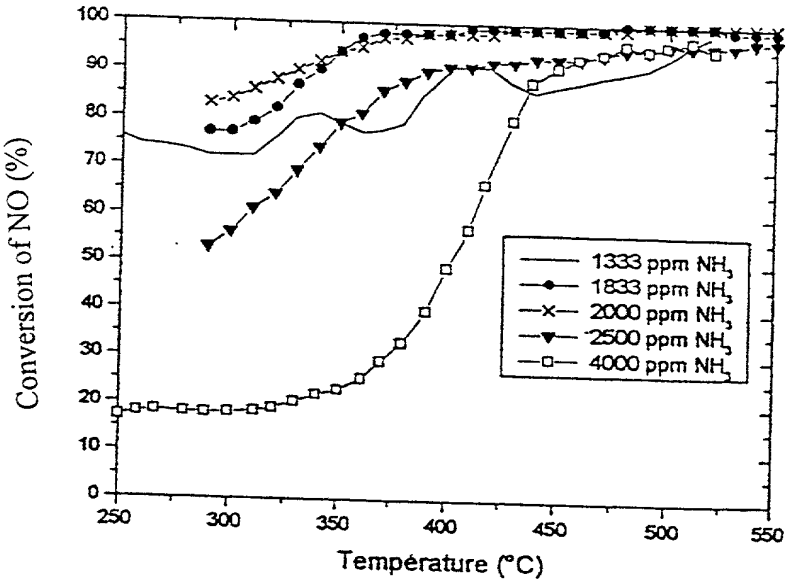

Fig. 3a: SCR of N_2O by NH_3 (2000 ppm/2000 ppm) in the presence of 3% 0_2 VVH = 35000 h^{-1}; Fe, H-BEA catalyst at different iron exchange rates

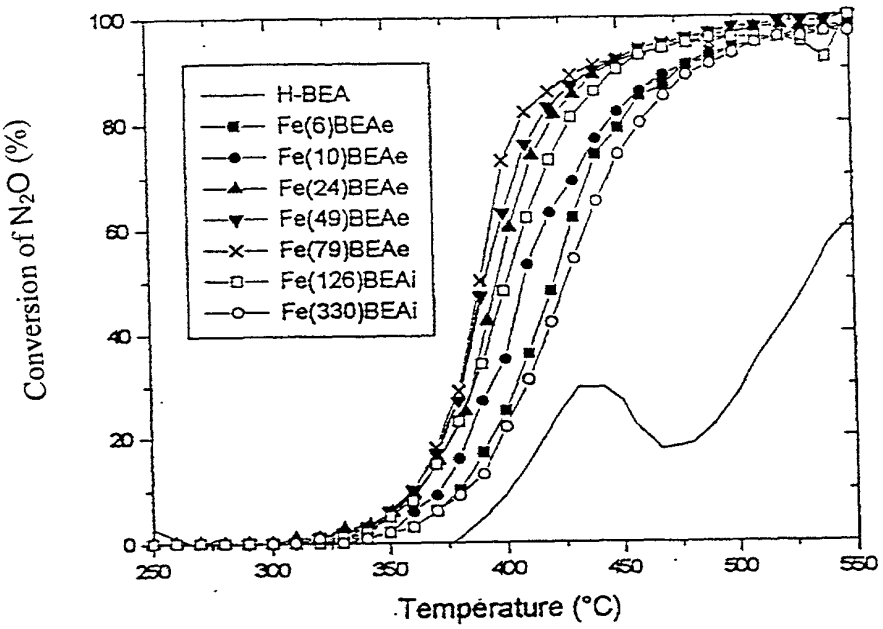

Fig. 3b: Influence of the iron content on the catalytic elimination of NO by NH_3 VVH = 10000 h^{-1}, 3% 0_2, 2000 ppm NO, 2000 ppm NH_3, He; descending temperature stage (1 hour every 10°C); catalyst: FeBEA at different and exchange rates

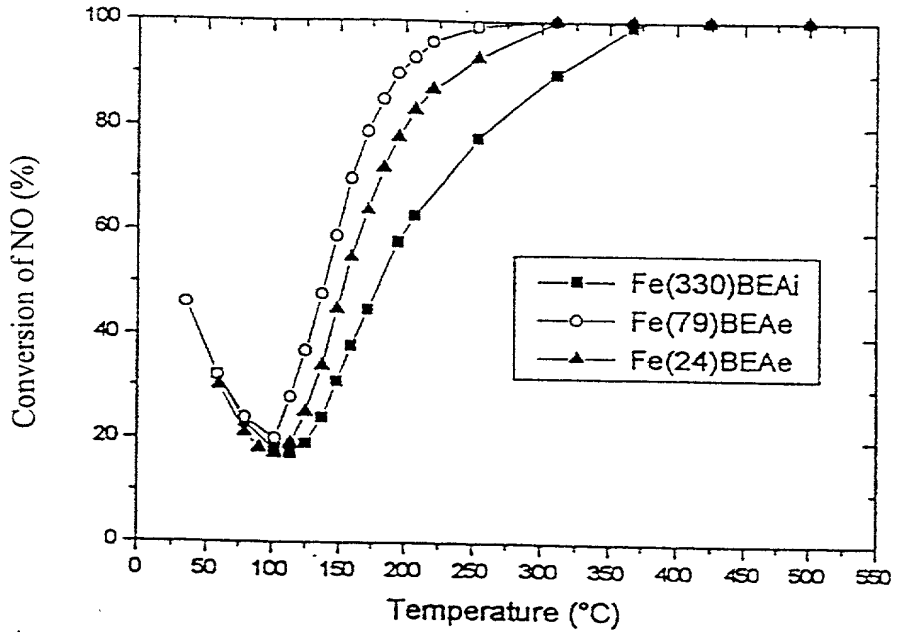

Fig. 3c: Simultaneous elimination of NO and N_2O on FeBEA
VVH = 10000 h^{-1}, 3% 0_2, 13500 pm H_2O, 1500 ppm NO, 1000 ppm N_2O, 2500 ppm NH_3, 1 hour stage every 10°C

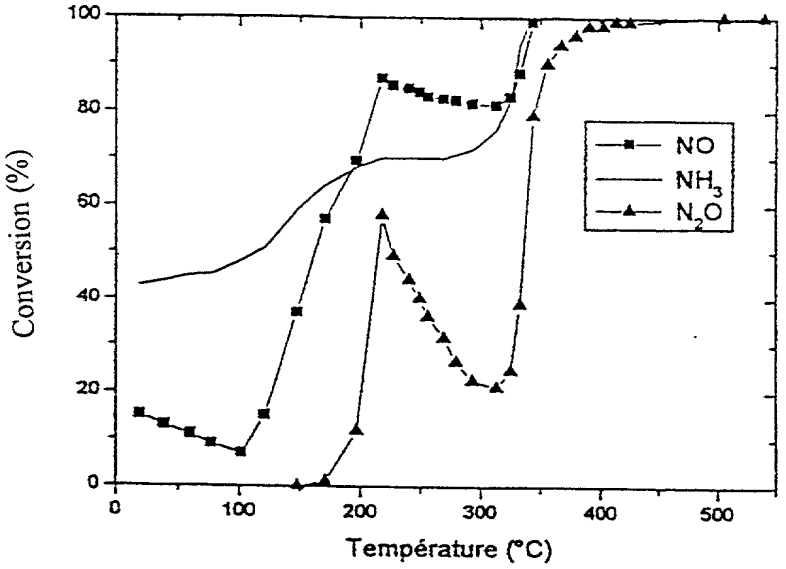

Fig. 4: Influence of the preparation method on SCR of N_2O + NO
VVH = 35000 h^{-1}, 3% 0_2, 2000 pm N_2O, 500 ppm NO, 1333 ppm NH_3; stage 1h/10°C
Catalyst: Fe(49) BEA_e; prepared by exchange and Fe(51) BEA; prepared by impregnation